SP-1301 US Serial No.: 10/625,820 September 29, 2008

Amendments to the Claims:

This listing of the claims will replace all prior versions and listings of claims in the application:

Listing of Claims

(Currently amended) A lecithin product, comprising:

phospholipids of up to about 75 wt.% of total dry matter wherein the phospholipids have a phosphatidyl-choline (PC) content of from 9 wt.% to 24.5 wt.% of total dry matter, a phosphatidyl-ethanolamine (PE) content of from 19.6 wt.% to 23 wt.% of total dry matter, and a phosphatidyl-inositol (PI) content of from 4 wt.% to 15 wt.% of total dry matter;

oil and sugar content of about 10 wt.% or less of total dry matter; and an acetone insolubles content of at least 72%;

wherein the lecithin product is prepared by a method comprising the steps of:

- (a) providing a crude lecithin material;
- (b) mixing the crude lecithin material with a blend of ethanol and water to form a first mixture, wherein a weight ratio of the crude lecithin material to the blend of ethanol and water is from about 1:1 to about 1:5 about 1:4:
 - (c) retaining solids from step (b);
- (d) mixing the retained solids in step (c) with a blend of ethanol and water to form a second mixture, wherein a weight ratio of the retained solids to the blend of ethanol and water is about 1:4: and
- (e) retaining solids from step (d) and drying the retained solids as an improved lecithin product;

wherein a weight ratio of ethanol to water in the blend of ethanol and water in at least one of steps (b) and (d) is from about 3:1 to about 1:3.

 (Original) The lecithin product of claim 1, wherein the weight percent of phospholipids is about 75 wt.% of total dry matter. Page 3

SP-1301 US Serial No.: 10/625,820 September 29, 2008

Canceled

(Original) The lecithin product of claim 1, wherein the product is granulated.

5-7 Canceled

 (Currently amended) A method for producing an improved lecithin product comprising the steps of:

- (a) providing a crude lecithin material;
- (b) mixing the crude lecithin material with a blend of ethanol and water to form a first mixture, wherein a weight ratio of the crude lecithin material to the blend of ethanol and water is from about 1:1 to about 1:5 about 1:4;
 - (c) retaining solids from step (b);
- (d) mixing the retained solids in step (c) with a blend of ethanol and water to form a second mixture, wherein a weight ratio of the retained solids to the blend of ethanol and water is about 1:4; and
- (e) retaining solids from step (d) and drying the retained solids as an improved lecithin product;

wherein the lecithin product has an oil and sugar content of about 10 wt.% or less of total dry matter; an acetone insolubles content of more than 72%, phospholipids of up to about 75 wt.% of total dry matter, and wherein the phospholipids have a phosphatidyl-choline (PC) content is from 9 wt.% to 24.5 wt.% of total dry matter, a phosphatidyl-ethanolamine (PE) content of from 19.6 wt.% to 23 wt.% of total dry matter, and a phosphatidyl-inositol (PI) content of from 4 wt.% to 15 wt.% of total dry matter:

wherein a weight ratio of ethanol to water in the blend of ethanol and water in at least one of steps (b) and (d) is from about 3:1 to about 1:3.

9-14 Cancelled

Page 4

SP-1301 US Serial No.: 10/625,820 September 29, 2008

- 15. (Original) The method according to claim 8, wherein steps (b) and (d) are preformed at a temperature of from about 12.8° C to about 68°C.
- 16. (Previously presented) The method according to claim 15, wherein step (b) and step (d) are preformed at a temperature of about 23°C, and in a high shear mixer.
- (Original) The method according to claim 16, wherein the solids are retained in steps
 (c) and (e) by centrifuging.
- (Original) The method according to claim 17, further comprising the step of drying the improved lecithin product.
- Canceled
- 20. (Original) The method according to claim 18, further comprising the step of granulating the improved lecithin product.
- (Previously presented) The method according claim 15, wherein step (b) and step
 (d) are preformed at a temperature of about 27°C to about 35°C, and in a low shear mixer.
- 22. (Original) The method according to claim 21, wherein the solids are retained in steps (c) and (e) by allowing the solids of step (c) and (e) to separate from liquid phase, and decanting the liquid phase.
- 23-27 Canceled